Bromine complexation agents in H₂/Br₂ flow battery cathodes: Physicochemical processes and

their influence on cell operation and cell performance

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Motivation for Cathodes in H_2/Br_2 RFB

Br

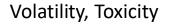
- Fast reaction kinetics at anode and cathode
- Energy density up 225 Wh L⁻¹ (6.7 M HBr)
- Bromine catholyte: reactand = electrolyte

Bromine storage as polybromide:

Catholyte: $Br_2 + Br^- \rightleftharpoons Br_3^-$

Catholyte: $xBr_2 + Br^- \rightleftharpoons Br_{1+2x}^-$

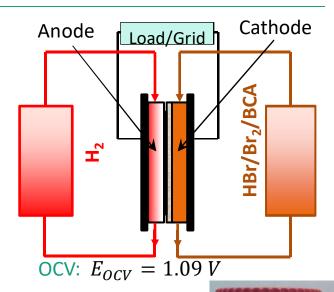
Challange of bromine cathode:





ammonium cations

Capture bromine in a separate phase



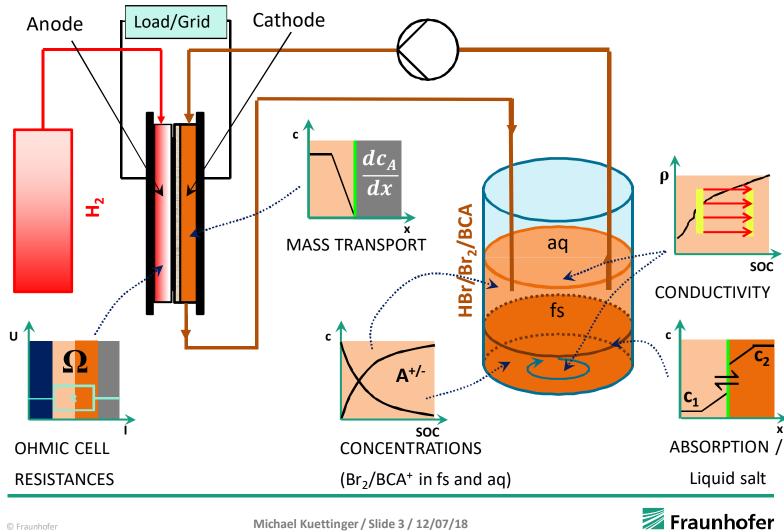
Ethylpyridiniumbromide: C₂PyBr SOC 0: 7.7 M HBr and 1.11 M C₂PyBr SOC 100: 1 M HBr; 3.35 M Br₂ and 1.11 M C₂PyBr



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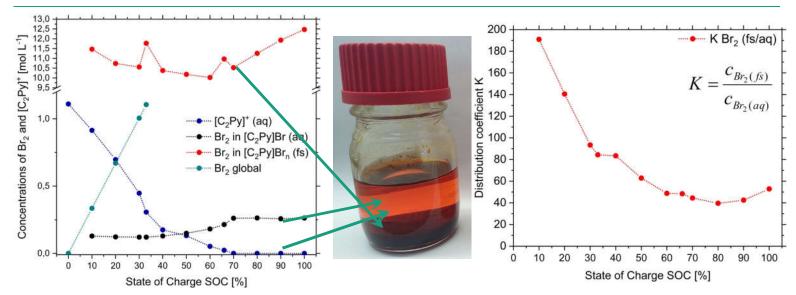


Influences of [C₂Py]Br on cell perf. at various SOC?

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How strong is Br₂ bound to [C₂Py]⁺?

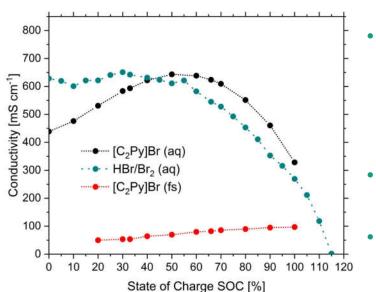


- Bromine concentration in fused salt around 11 M Br₂ >>> 640 Wh L⁻¹
- Strong complexation of Br₂ with [C₂Py]⁺ ... 0.35 M Br₂ vs. 3.35 M Br₂ at SOC 100 leading to a safer catholyte

$$BCA^+(aq) + Br^-(aq) + xBr_2(aq) \rightleftharpoons BCABr_{2x+1}(fs)$$

 Complexation of Br₂ with C2Py⁺ leads to falling C2Py⁺ concentration in aqueous phase





Conductivity of catholyte aq + fs

 Fused salt phase showing conductivities between 45 and 90 mS cm⁻¹

- Conductivities of pure HBr/Br₂/H₂O phase at around 625 mS cm⁻¹ for SOC 0 to SOC 50 and falling for SOC > 60. The proton amount in the electrolyte falls due to cell reaction.
 - C₂Py⁺ limits the conductivity in accordance to concentration plot (445 mS cm⁻¹)
 - Complexation of C₂Py⁺ with Br₂ and extraction of fused salt leads to rising conductivities for SOC 0 (445 mS cm⁻¹) to SOC 60 (643 mS cm⁻¹)

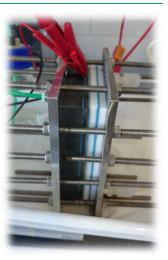
Bromine extraction:

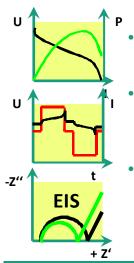
 $BCA^{+}(aq) + Br^{-}(aq) + xBr_{2}(aq)$ $\Rightarrow BCABr_{2x+1}(fs)$

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$H_2/Br_2 RFB - Celltest with C_2Py^+$

- Bromine cathode aqueous phase pumped around
 - Graphite felt (GFA 5, SGL, Carbon, D)
 - Current collector Glassy Carbon (Sigradur G, HTW, D)
- Hydrogen anode / MEA- 40 cm² active area (membrane)
 - Nafion 117[®], 3 mg Pt cm⁻² on carbon cm² surface) + GDL (BC 25, SGL Carbon, D)
 - 100 mL min⁻¹ H₂ flow (nonrecyclable)



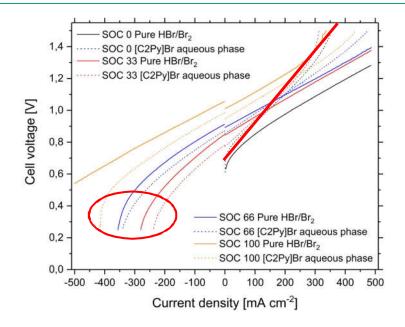


- Linear sweep potentiometry: +/- 1.25 mA cm⁻² s⁻¹ in the range of 0 to 500 mA cm⁻² threshold points: 0.25 V and 1.5 V
- Galvanostatic cycling test +/- 50 mA cm⁻²; threshold points: 0.25 V and 1.5 V including detection of half cell potentials and redox potential of the catholyte
- Ohmic cell resistances by galvanostatic electrochemical impedance spectroscopy (EIS) Amplitude: +/- 10 mA cm⁻²

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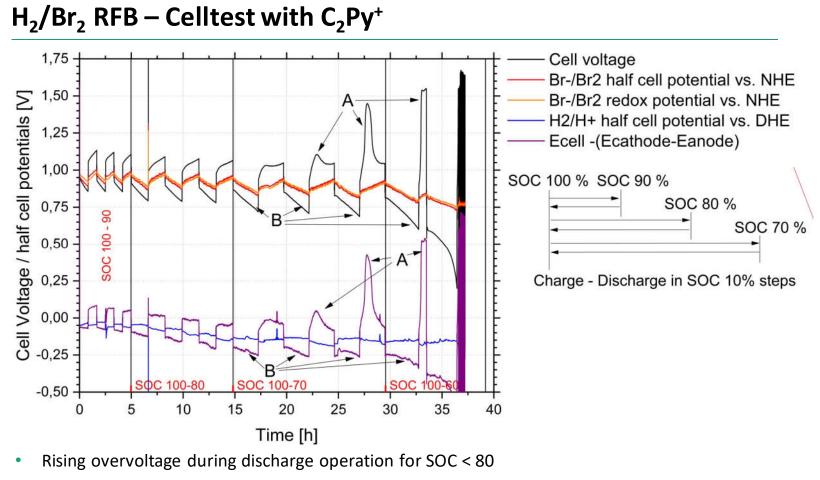
Linear sweep potentiometry with C₂Py⁺ and without



- Discharge LSP limited by mass transport limitation: c(Br₂) lower for C₂Py⁺
- Charge LSP with high ohmic resistances for SOC 0 % (2.2 Ohm cm²) and SOC 33 % (2.4 Ohm cm²), compared to SOC 66 % (0.93 Ohm cm²) and SOC 100 % (0.81 Ohm cm²).







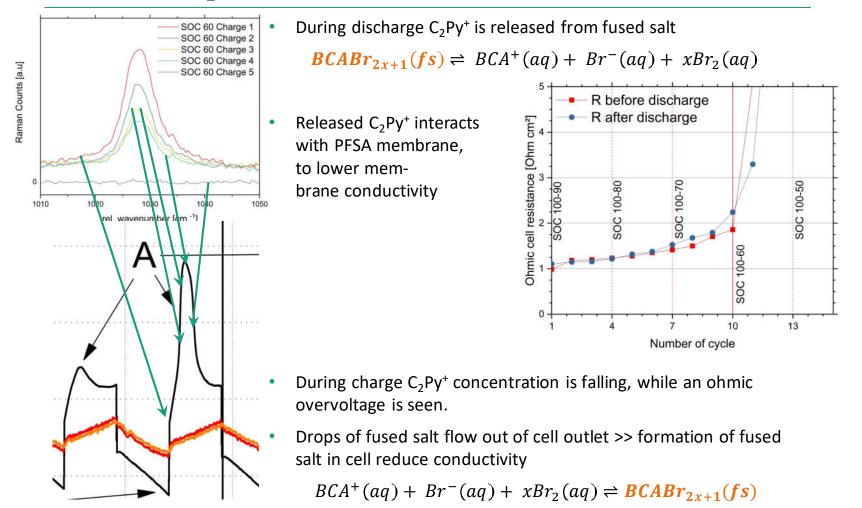
- Overvoltage peak during charge process (time dependent)
- Neither anodic potential nor cathodic potential follow these trends

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Influence of C₂Py⁺ cations on cell performance

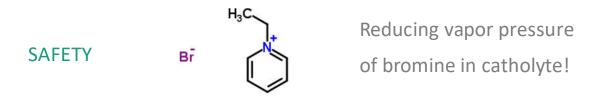


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Conclusion



 Composition of electrolyte acts as an important parameter on the performance for the investigated H₂/Br₂ single cell

HIGH C₂Py⁺ concentrations in aqueous phase lead to

- Decrease of conductivity
- Rising membrane resistance
- Formation of fused salt in cathode (lower conductivity)
- Limiting range of usable SOC to 30%

Got information about processes in cell limiting the PERFORMANCE

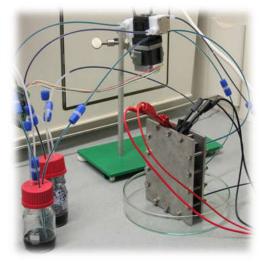
Different operation modes and electrolyte formulations shall limit the influence of C_2Py^+ , while offering a safe catholyte

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THANK YOU FOR YOUR ATTENTION !!





Michael Kuettinger

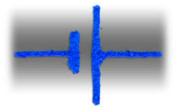
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